

## 國立臺灣科技大學 110 學年度碩士班招生試題

系所組別：化學工程系碩士班  
 科目：化工熱力學與動力學

(總分為 100 分)

- (15%) The pressure derivative of entropy at the constant temperature is written in terms of  $-\left(\frac{\partial v}{\partial T}\right)_P$ . If liquid ammonia at 350 K is compressed from saturation pressure of 270 kPa to 1000 kPa, determine its enthalpy ( $\Delta H$ , kJ/kg) and entropy ( $\Delta S$ , kJ/kg·K) changes. For saturated liquid ammonia at 350 K, liquid volume and volume expansivity ( $\beta$ ) are  $1.551 \times 10^{-3} \text{ m}^3 \cdot \text{kg}^{-1}$  and  $2.095 \times 10^{-3} \text{ K}^{-1}$ , respectively.
- (15%) Air (molar mass = 28.851 g/mol) enters a compressor through a 5-cm-radius tube with an average velocity of  $10 \text{ m} \cdot \text{s}^{-1}$  at the initial conditions [ $P_1 = 1 \text{ bar}$  and  $T_1 = 10^\circ\text{C}$ ], and is discharged through a 1.5-cm-radius tube at the final conditions [ $P_2 = 36 \text{ bar}$  and  $T_2 = 90^\circ\text{C}$ ]. The shaft work supplied to the compressor is  $25.0 \text{ kJ} \cdot \text{mol}^{-1}$ . Determine the heat-transfer rate (kJ/sec) from the compressor? Assume enthalpy and specific volume at initial condition are  $30.68 \text{ kJ} \cdot \text{mol}^{-1}$  and  $31.40 \text{ L} \cdot \text{mol}^{-1}$ , respectively, while enthalpy and specific volume at final condition are  $33.97 \text{ kJ} \cdot \text{mol}^{-1}$  and  $0.5438 \text{ L} \cdot \text{mol}^{-1}$ , respectively.
- (10%) If volumetric equation of state ( $P = \frac{RT}{V} - \frac{a-bRT^{3/2}}{\sqrt{TV^2}}$ ) can be expanded in the form of Virial equation of state, show that Boyle temperature ( $T_B$ ) for the volumetric equation of state is written in terms of  $a$ ,  $b$ , and  $R$ .
- (10%) A refrigeration system cools a steel casting from  $25^\circ\text{C}$  to  $-15^\circ\text{C}$  at a rate of  $15 \text{ kg} \cdot \text{s}^{-1}$ . Assume that heat flows from the refrigeration system to the surroundings at a temperature of  $45^\circ\text{C}$  and the specific heat capacity of the steel casting is  $7.6 \text{ kJ} \cdot \text{kg}^{-1} \cdot ^\circ\text{C}^{-1}$ . If the thermodynamic efficiency of the process is 31%, determine the power (kJ/kg) requirement of the system?
- (12%) A liquid-phase reaction  $A \rightarrow 2R$  was performed in a CSTR with a volume of 5 L. In the reaction, the reactant A was fed to the CSTR at a concentration of 1 mol/L. The researcher intended to find a rate expression for this reaction by carrying out the experiments at different conditions, which were summarized in the following Table. Please determine the **reaction order** and the **activation energy** of this reaction.

Run	Feed rate ( $\text{cm}^3/\text{s}$ )	Reaction temperature ( $^\circ\text{C}$ )	Concentration of R in effluent (mol/L)
#1	2	13	1.8
#2	15	13	1.5
#3	15	84	1.8



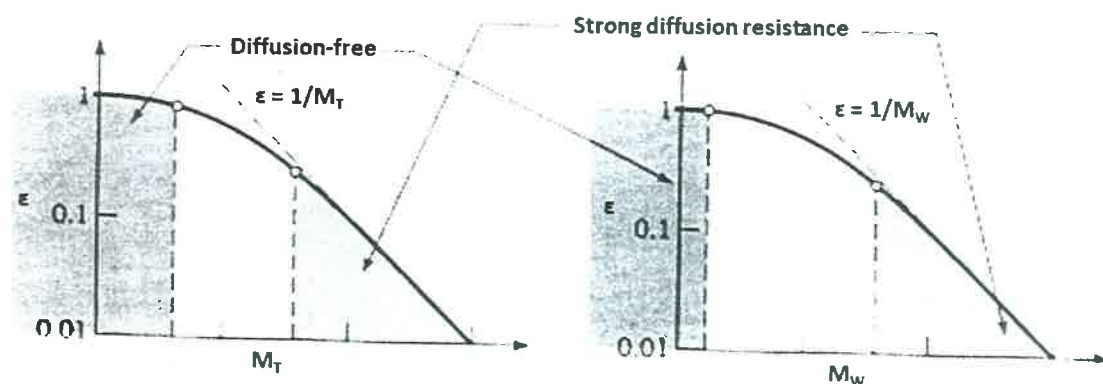
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6. (15%) An experimental rate measurement on the decomposition of A is made with a particular catalyst. For the spherical particle:  $d_p = 2.4$  mm,  $D_e = 5 \times 10^{-5}$  m<sup>2</sup>/hr (Effective mass conductivity),  $k_{eff} = 1.6$  kJ/hr-m cat-K (Effective thermal conductivity), for the gas film surrounding the pellet:  $h = 160$  kJ/hr-m<sup>2</sup> cat-K (heat transfer coefficient),  $k_g = 300$  m<sup>3</sup>/hr-m<sup>2</sup> cat (mass transfer coefficient), for the reaction:  $\Delta H_r = -160$  kJ/mol A (exothermic),  $C_{Ag} = 20$  mol/m<sup>3</sup> (at 1 atm, 336 °C),  $-r''_{A,obs} = 10^5$  mol/hr-m<sup>3</sup> cat.

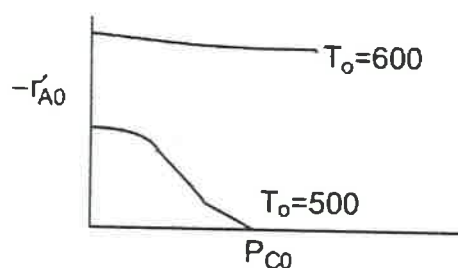
- Is it likely that film resistance to mass transfer influence the rate? (5%)
- Could this run have been made in the regime of strong pore diffusion? (5%)
- Would you expect to have temperature variations within the pellet or across the gas film? (5%)



$M_r$ : Thiele modulus,  $M_w$  = Wagner-Weisz-Wheeler modulus,  $\epsilon$  = effectiveness factor, (actual mean reaction rate within pore)/(rate if not slowed by pore diffusion)

7. (11%) In an ammonia decomposition reaction to generate N<sub>2</sub> and H<sub>2</sub> on a Platinum catalyst ( $2\text{NH}_3 \rightarrow \text{N}_2 + 3\text{H}_2$ ) the rate can be expressed as  $-r = kK_A P_A / K_H P_H$ , where  $k$  is the rate constant,  $P_A$  and  $P_H$  indicate the pressures of ammonia and hydrogen, and  $K_A$  and  $K_H$  are the adsorption constants for ammonia and hydrogen. Suggest a **mechanism** and the **assumptions** consistent with the rate equation and prove it.

8. (12%) The irreversible gas phase reaction of A and B to form C and D was carried out in a packed bed reactor in which there is no catalyst decay. The following figure shows the rate of reaction at the reactor entrance as a function the partial pressure of C for various entering temperatures,  $T_0$  (K).



Choose the one best answer from the information given for the above system:

- The reaction is exothermic: (1) True, (2) False, (3) Cannot tell (3%)
- The reaction is endothermic: (1) True, (2) False, (3) Cannot tell (3%)
- Species C is adsorbed on the catalyst surface at 400 K: (1) True, (2) False, (3) Cannot tell (3%)
- Species C is adsorbed on the catalyst at 700 K: (1) True, (2) False, (3) Cannot tell (3%)

